

Separation Processes, ChE 4M3, 2013

Assignment 5

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Due date: 03 December 2013 (no late handins)

Objectives: Understanding liquid-liquid extraction systems, adsorption, and drying.

Question 1 [20]

A stream of acetic acid and water (also called diluent) is being fed in a counter current manner at 1000 kg/hour, in order to extract the acetic acid. The feed composition is 30 wt% acetic acid, and 70 wt% water.

The solvent is 99% pure IPE (isopropyl ether), and contains 1% acetic acid, at an inlet flow of 2500 kg/hour.

We desire the exiting raffinate stream to contain 5 wt% acetic acid.

1. Find the number of equilibrium stages to achieve this separation (show all calculations).
2. Calculate the exiting raffinate flow, and the exiting extract flow rate.

Unfortunately, we don't have the equilibrium data, however, various samples of the 3 species were made, mixed, and when they came to equilibrium they were found to have the following compositions (each row gives the aqueous and organic phase compositions):

Aqueous phase (weight %)			Organic phase (weight %)		
IPE	Water	Acetic acid	IPE	Water	Acetic acid
1.2	98.1	0.7	99.5	0.5	0
1.5	97.1	1.4	99.0	0.7	0.3
1.6	95.5	2.9	98.5	0.8	0.7
2.0	91.7	6.3	97	1	2
2.5	84.5	13	93	2	5
3	71	26	84	4	12
4	59	37	72	7	21
10	45	45	58	11	31
16	37	47	49	15	36

Feel free to download and use [this empty ternary diagram](#). Electronic submissions that are based on photos are not acceptable, unless the photo is perpendicular to the page, and every detail is clear. If in doubt, submit your assignment in paper form.

Question 2 [11 = 2 + 2 + 2 + 2 + 3]

1. What is the dew point temperature of an air stream containing 15% humidity at 70°C?
2. What is the amount of water carried in 5 kg of this stream?
3. This stream is cooled adiabatically; what is the adiabatic saturation temperature?
4. What is the amount of moisture held now, after this adiabatic cooling?
5. What is the wet-bulb temperature, dew point temperature, and percentage humidity of an air stream at 90°C and containing 100 grams of water per kilogram of dry air?

Question 3 [10 = 6 + 4]

From the final exam, 2012.

An undesirable solute is to be removed from 20 m³ of liquid by contacting it with a batch of adsorbent. The adsorption of the solute on the adsorbent follows a Langmuir type adsorption isotherm:

$$C_{A,S} = \frac{1.5C_A}{0.5 + C_A}$$

where C_A is measured in kg.m⁻³ and $C_{A,S}$ is in kg.kg⁻¹. The concentration of the solute in the feed liquid is 0.1 kg.m⁻³ when it is first charged to the batch reactor.

1. How much adsorbent will be needed to reduce the solute concentration in the liquid to 0.01 kg.m⁻³? And what mass of solute is loaded onto the adsorbent?
2. Describe an experimental procedure (use bullet points) that will provide the data necessary to fit the two coefficients in the Langmuir isotherm. Note, do not provide details how to numerically calculate the coefficients, only describe the exact procedure to obtain a data table of C_A and $C_{A,S}$ values.

Question 4 [24 = 2 + 2 + 4 + 10 + 4 + 2]

From the final exam, 2012.

A cylindrically-shaped food product (e.g. snack food, or pet food) that is 0.5cm in diameter and 2cm in length according to the product requirements, is extruded with a moisture content of 35% on a dry basis. These extruded pellets are to be dried to 8% dry basis to obtain the correct level of consistency for flowability and long-term storage, another product requirement. Drying air is available from an facility at your site, and is rated at 30% humidity and 70°C; this is provided at a velocity of 3 m.s⁻¹ in the batch drier. The mass of moist material is 150 kg, and corresponds to about 50,000 pellets per tray.

Heat transfer coefficients for drying are estimated from correlations. For a packed bed, a correlation by Gamson, Thodos and Hougen in *AICHE Journal*, **39**, p 1 – 35, 1943 where:

- h is the heat transfer coefficient, in [W.m⁻².K⁻¹]
- G is the mass flux of air, in [kg.hr⁻¹.m⁻²]
- d_p is the particle size diameter [m], for spherical particles, are then used in the following equation:

$$h = 0.151 \frac{G^{0.59}}{d_p^{0.41}}$$

1. Explain why food products often require a specific level of dryness.
2. Since these particles are not spherical, *justify* a suitable equivalent-particle diameter to use as d_p in the above heat transfer correlation.
3. Now *calculate* this equivalent-particle diameter.
4. Calculate the drying time required *in minutes*. State any assumptions made.

Note: for packed beds, it is common practice to use only 50% of the external air stream velocity as the effective velocity within the packed bed.

5. This correlation requires the packed bed Reynolds number, $N_{Re} = \frac{d_p G}{\mu} > 350$, where the air's viscosity is approximately $2 \times 10^{-5} \text{ kg.m}^{-1}.\text{s}^{-1}$. Is this condition met? Note that G must be expressed in SI units for calculating the Reynolds number.
6. Describe a parameter you could adjust on the drier to decrease the drying time, and why your change would work. You can consider minor capital expenditure to implement this change.
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END