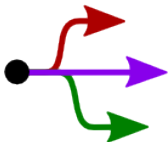


Separation Processes

ChE 4M3



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<http://learnche.mcmaster.ca/4M3>

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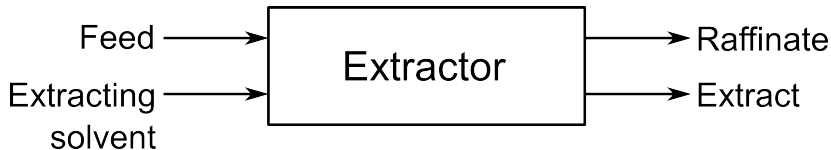
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Liquid-liquid extraction (LLE)



[Flickr# 3453475667]

Definitions



- ▶ **solute**: species we aim to recover (A) from the feed
- ▶ **feed or “feed solvent”**: one of the liquids in the system (“carrier”)
- ▶ **solvent**: MSA (by convention: the “added” liquid)
- ▶ **extract**: solute mostly present in this layer = y_A
- ▶ **raffinate**: residual solute in this layer = x_A
- ▶ **distribution**: how the solute **partitions** itself = $D_A = \frac{y_A}{x_A} = \frac{y_E}{x_R}$
 - ▶ measure of affinity of solute
 - ▶ $D_A = \frac{\mu_R^0 - \mu_E^0}{RT} = \frac{\text{chemical potential difference}}{(R)(\text{temperature})}$

Where/why LLE is used

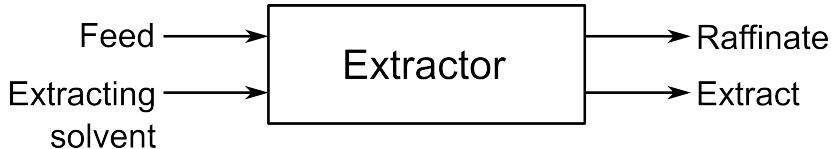
Where?

- ▶ Bioseparations
- ▶ Nuclear (uranium recovery)
- ▶ Mining: nickel/cobalt; copper/iron
- ▶ Perfumes, fragrances and essential oils
- ▶ Fine and specialty chemicals

Why?

- ▶ Temperature sensitive products
- ▶ High purity requirements
- ▶ High-boiling point species in low quantity
- ▶ Need to separate by species type (rather than relative volatility)
- ▶ Close-boiling points, but high solubility difference
- ▶ Azeotrope-forming mixtures

Extractor types



1. Mixing/contacting:

- ▶ turbulent contact between liquid phases
- ▶ small droplet **dispersion** in a **continuous** phase
 - ▶ which phase is dispersed?
- ▶ mass-transfer between phases
- ▶ limited by solute loading in solvent

2. Phase separation:

- ▶ reverse of mixing step
- ▶ drops coalesce
- ▶ relies on density difference

3. Collection of phases leaving the unit

What are we aiming for?

Main aims

- ▶ High recovery of solute overall (low x_R and high y_E)
- ▶ Concentrated solute in extract (high y_E)

How to achieve this?

- ▶ Counter-current mixer-settlers in series
 - ▶ High interfacial area during mixing
 - ▶ Reduce mass-transfer resistance
 - ▶ Promote mass transfer
 - ▶ molecular diffusion
 - ▶ eddy diffusion
- ← orders of magnitude greater

Equipment for LLE

1. Mixer-settlers

- ▶ mix: impellers
- ▶ mix: nozzles
- ▶ mix: feeds meet directly in the pump
- ▶ mix: geared-teeth devices
- ▶ main aim: good contact; avoid droplets smaller than $2\text{ }\mu\text{m}$
- ▶ settle: baffles, membranes
- ▶ settle: ultrasound
- ▶ settle: chemical treatment
- ▶ settle: centrifuges

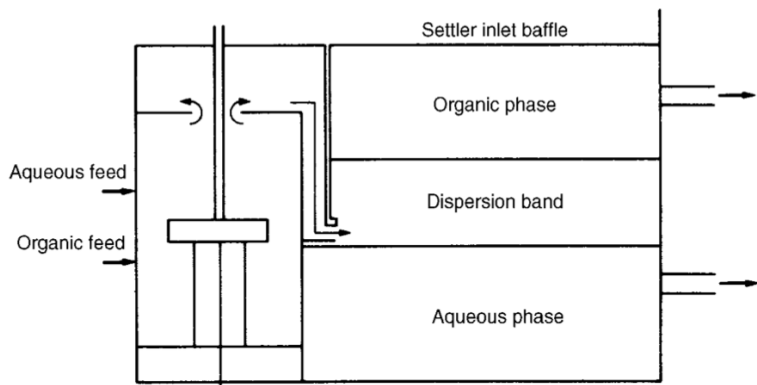
2. Columns with:

- ▶ (a) nothing or
- ▶ (b) trays and/or
- ▶ (c) packing and/or
- ▶ (d) pulsating and/or
- ▶ (e) agitation

3. Rotating devices

Important point: LLE is an equilibrium-limited separation (as opposed to rate limited separations seen up to now).

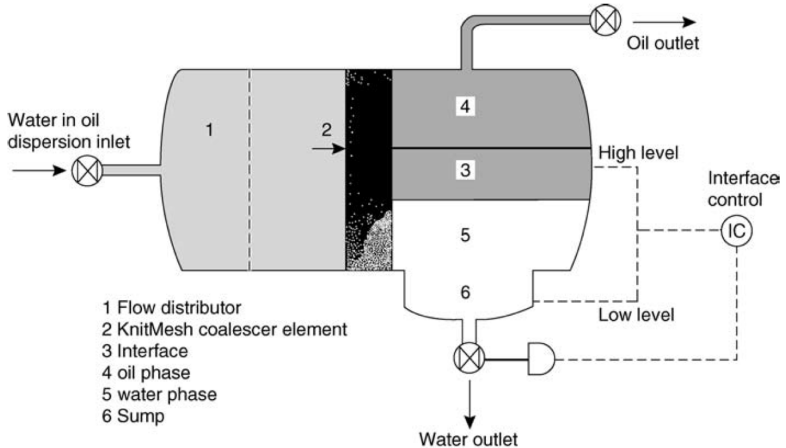
Mixer-settlers



[Richardson and Harker, p 745] Common in mining industry: requirements
~40000 L/min flows

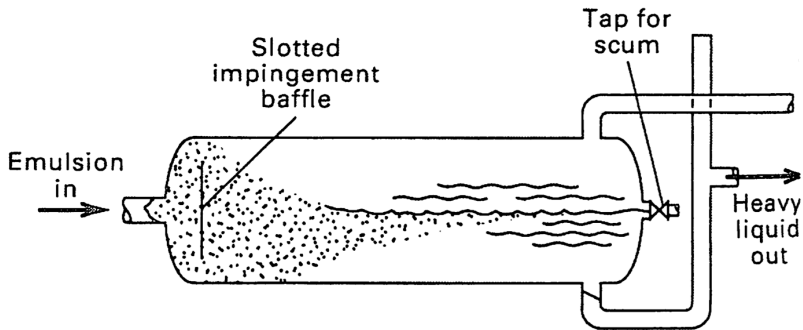
Mixer-settlers

KnitMesh coalescer: consistency of “steel wool”



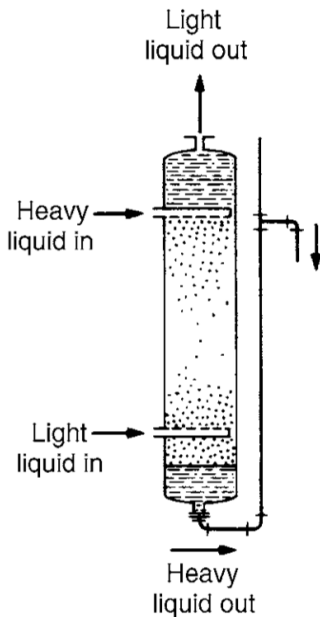
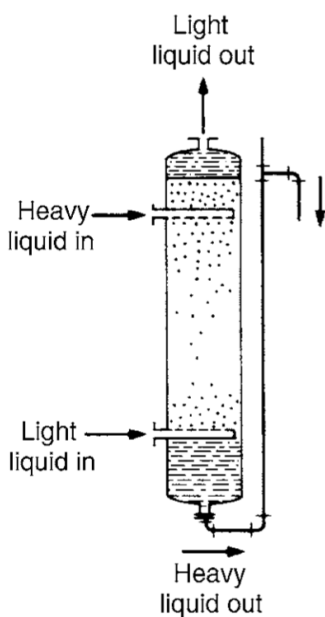
[Richardson and Harker, p 747]

Horizontal gravity settling vessel

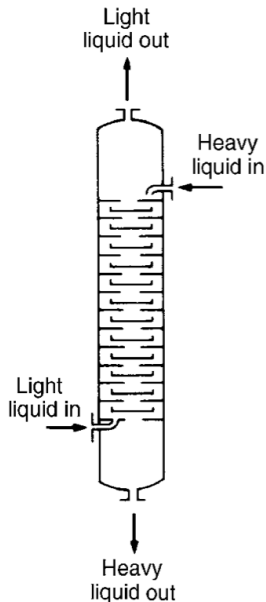
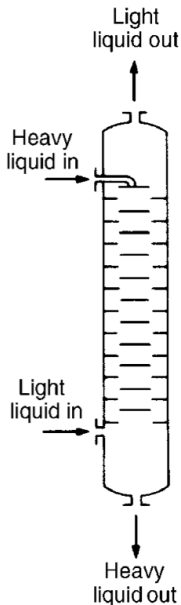


[Seader, 3ed, p302]

Spray columns: separation principle is gravity

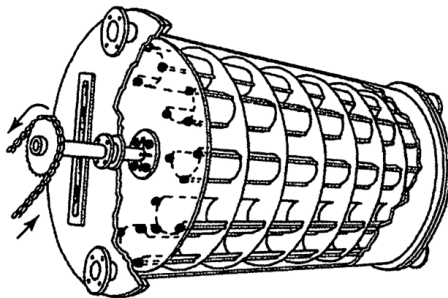


Tray columns



- ▶ coalescence on each tray
- ▶ tray holes: $\sim 3\text{mm}$
- ▶ breaks gradient formation (axial dispersion)

Rotating devices

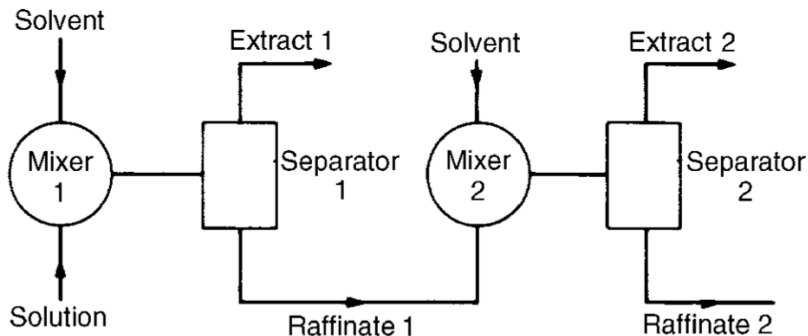


[Seader, 3ed, p 306]

- ▶ “white” = lighter liquid
- ▶ “grey” = heavier liquid

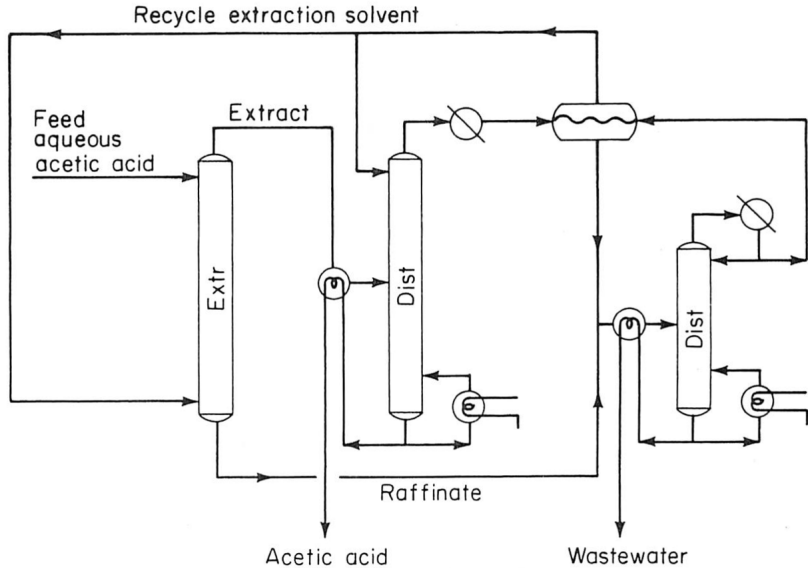
Used when foams and emulsions would easily form: i.e. gentle mass transfer.

Linking up units (more on this later)



[Richardson and Harker, p 723]

Integration with downstream units



Selecting a solvent

Schweitzer: “The **choice of solvent** for a LLE process can often have a more significant impact on the process economics than any other design decision that has to be made”.

Which properties of a solvent influence our aims with LLE?

- ▶ High distribution coefficient (selectivity) for solute



Calculating the distribution coefficient

Mass balance:

$$F x_F + S y_S = E y_E + R x_R$$

$$D = \frac{y_E}{x_R}$$

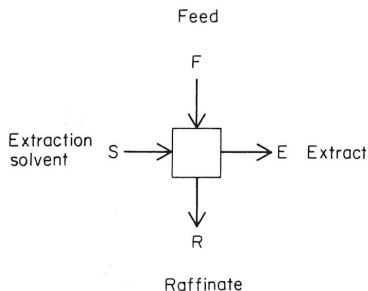
If $F = S = E = R$ and $y_S = 0$, then
only measure x_R :

$$D = \frac{x_F}{x_R} - 1$$

- ▶ Capital letters refer to mass amounts
- ▶ y_{\square} ← refers to mass fractions in solvent layer
- ▶ x_{\square} ← refers to mass fractions in carrier and extract layers

Once D is determined, we can obtain phase diagrams to understand how the process will operate.

Also: see Perry's for many values of D

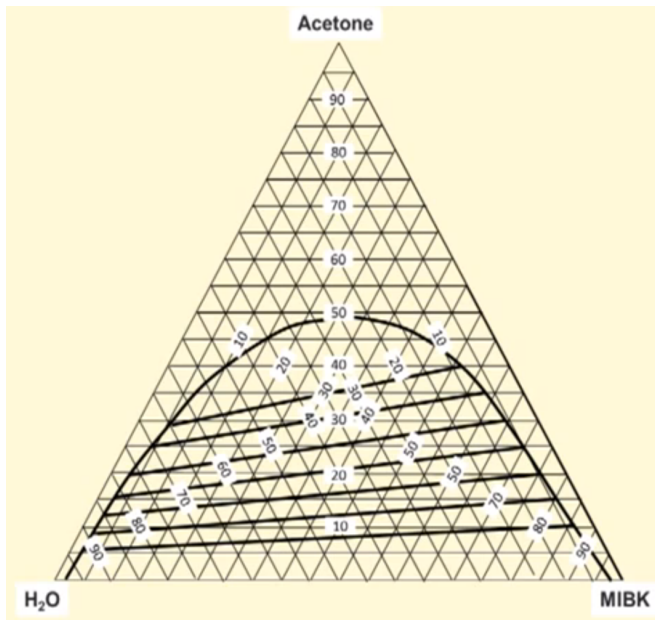


Triangular phase diagrams: from laboratory studies

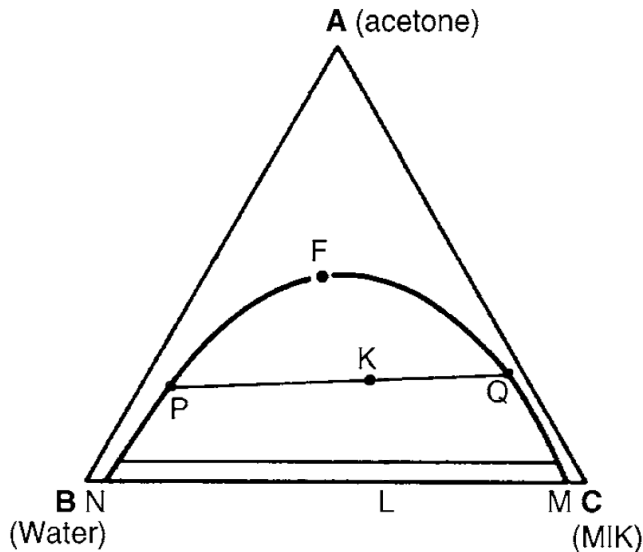


[Flickr# 3453475667]

Using a triangular phase diagrams



Lever rule



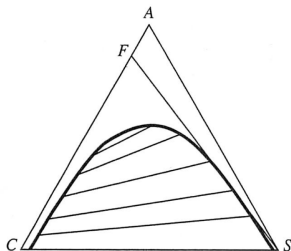
Mix P and Q

- ▶ mixture = K
- ▶ $\frac{PK}{KQ} = \frac{\text{amount Q}}{\text{amount P}}$
- ▶ The converse applies also:
when separating a settled mixture
- ▶ Applies anywhere:
even in the miscible region

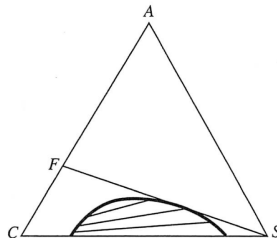
Q1: Using the lever rule

Which is a more or effective system?

- ▶ S = pure solvent used
- ▶ F = feed concentration



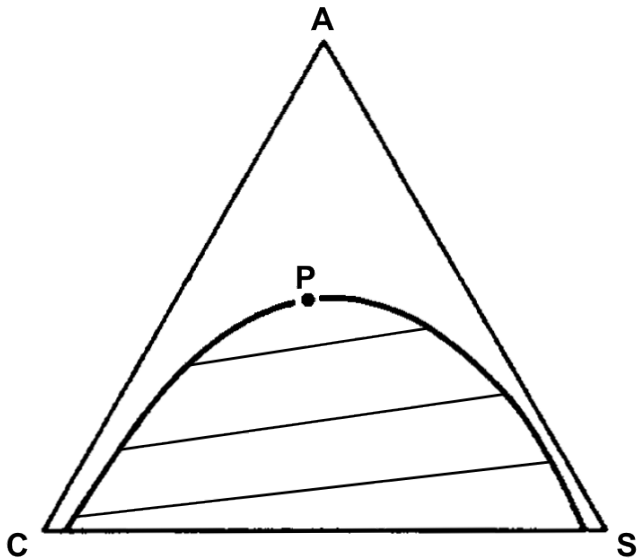
(a)



(b)

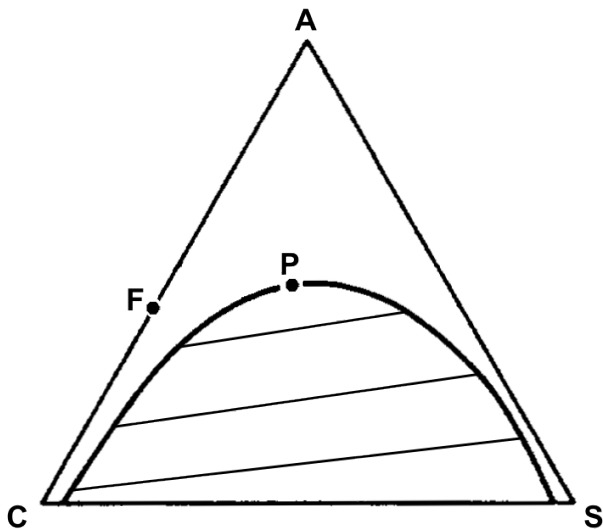
Answer:

Q2: Using the lever rule



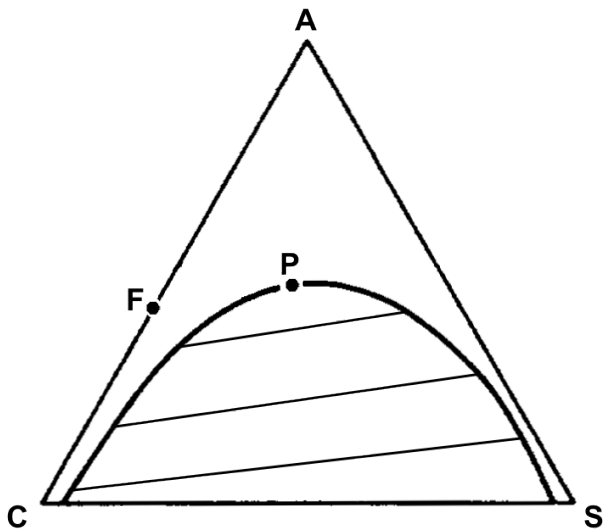
Which is a more effective as a solvent: C or S ?

Q3: Using the lever rule



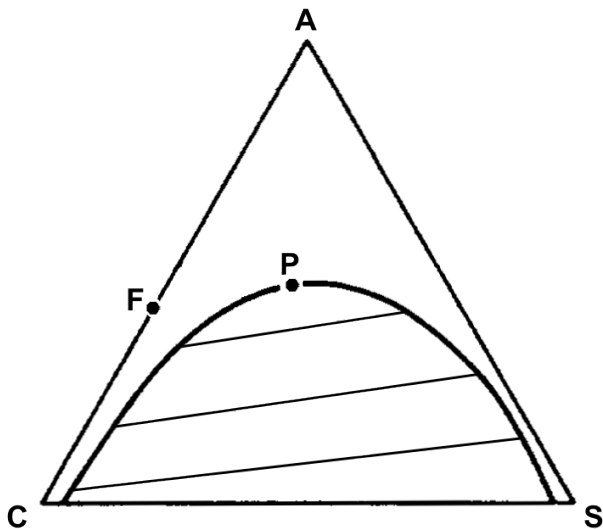
Mix a feed stream, F , containing C and A (i.e. x_f) with a pure solvent stream S (i.e. $y_S = 0$). Composition of the mixture?

Q4: Going to equilibrium



Let that mixture M achieve equilibrium. What is the composition of the raffinate and extract?

Q5: Altering flows



Same system, but now lower solvent flow rate (to try save money!). What happens to (a) extract concentration and (b) solute recovery?

References

- ▶ Schweitzer, "Handbook of Separation Techniques for Chemical Engineers", Chapter 1.9
- ▶ Seader, Henly and Roper, "Separation Process Principles", 3rd edition, chapter 8
- ▶ Richardson and Harker, "Chemical Engineering, Volume 2", 5th edition, chapter 13
- ▶ Geankoplis, "Transport Processes and Separation Process Principles", 4th edition, chapter 12.5
- ▶ Ghosh, "Principles of Bioseparation Engineering", chapter 7
- ▶ Uhlmann's Encyclopedia, "Liquid-Liquid Extraction",
[DOI:10.1002/14356007.b03_06.pub2](https://doi.org/10.1002/14356007.b03_06.pub2)