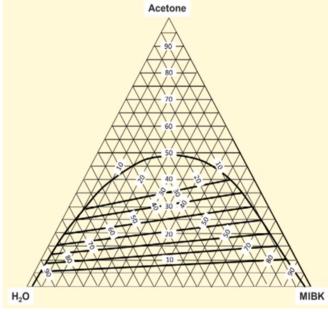
Triangular phase diagrams: from laboratory studies

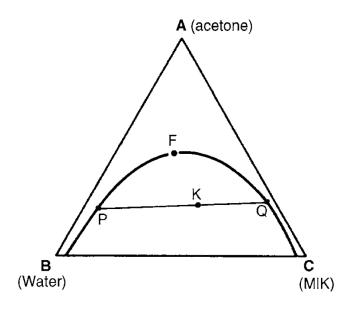


[Flickr# 3453475667]

Using a triangular phase diagrams



Lever rule



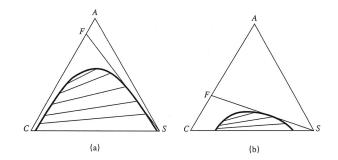
Mix P and Q

- mixture = K
 - $\frac{\mathsf{PK}}{\mathsf{KQ}} = \frac{\mathsf{amount Q}}{\mathsf{amount P}}$
- The converse applies also: when separating a settled mixture
- Applies anywhere: even in the miscible region

Q1: Using the lever rule

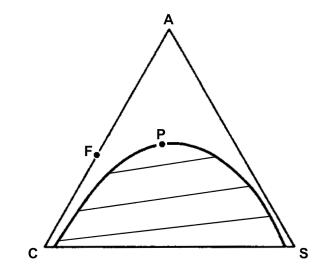
Which is a more *flexible* system?

- S = pure solvent used
- F = feed concentration point (more correctly it is x_F)



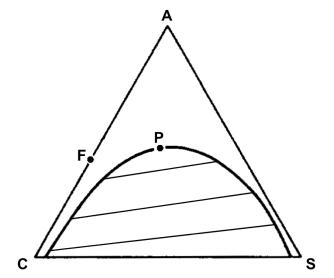
Answer:

Q2: Using the lever rule



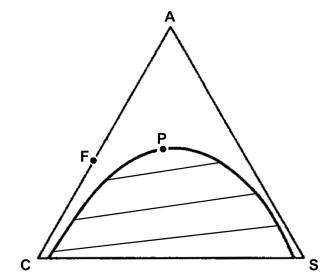
Mix a feed stream, F, containing C and A (i.e. x_F) with a pure solvent stream S (i.e. $y_S = 0$). Composition of the mixture?

Q3: Going to equilibrium



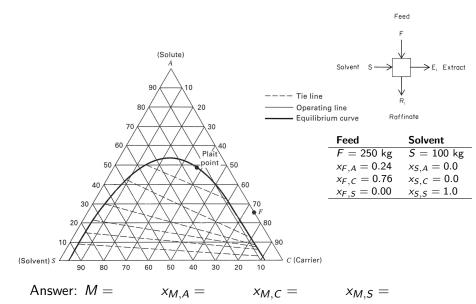
Let that mixture M achieve equilibrium. What is the composition of the raffinate and extract?

Q4: Altering flows

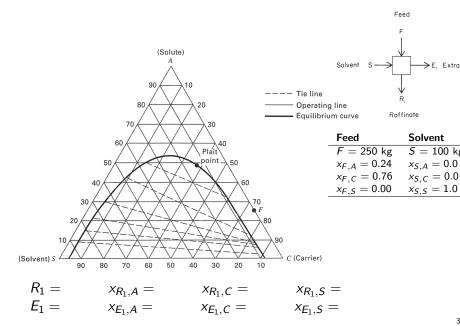


Same system, but now lower solvent flow rate (to try save money!). What happens to (a) extract concentration and (b) solute recovery?

Q5: Composition of the mixture, M?



Q6: Composition of the 2 phases leaving in equilibrium?



33

Feed

→E, Extract

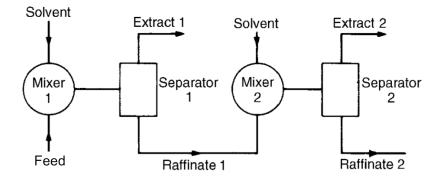
Solvent

S = 100 kg

 $x_{S,A} = 0.0$

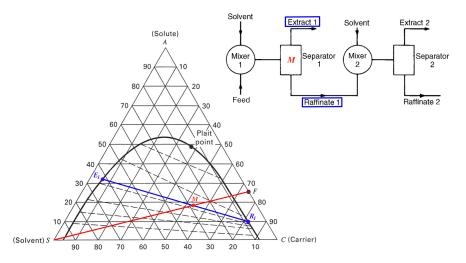
 $x_{5,5} = 1.0$

Link units in series



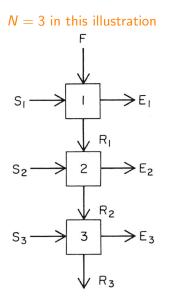
[[]Richardson and Harker, p 723]

Q7: send raffinate from Q6 to second mixer-settler



Question: how much solvent should we use in the second stage?

Series of co-current units



 Recovery = fraction of solute recovered

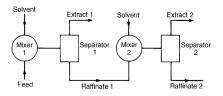
$$1-\frac{(x_{R_N})(R_N)}{(x_F)(F)}$$

 Concentration of overall extract = solute leaving in each extract stream, divided by total extract flow rate

$$\frac{\sum_{n}^{N} (y_{E_n})(E_n)}{\sum_{n}^{N} E_n}$$

Schweitzer, p 1-263

Co-current vs counter-current Co-current (N = 2 stages)



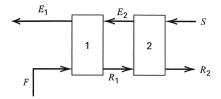
- $\begin{array}{c|c} & & & & \\ & & & \\ & & & \\ & & & \\ F \end{array} \xrightarrow{E_2} & & S \\ & & & & \\ & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & &$
- We combine multiple extract streams
- (Only 2 in illustration)
- In general: $y_{E_1} > y_{E_2} > \dots$
- Fresh solvent added at each stage

- "Re-use" the solvent, so
- Far lower solvent flows
- Recovery = $1 \frac{(x_{R_N})(R_N)}{(x_F)(F)}$
- Concentration = y_{E_1}

You will have an assignment question to compare and contrast these two configurations

Counter-current (N = 2 stages)

Some theory: Two counter-current units



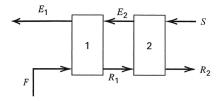
Just consider N = 2 stages for now. Steady state mass balance: $F + E_2 = E_1 + R_1$ $E_2 + R_2 = S + R_1$

Rearrange:

$$F - E_1 = R_1 - E_2$$

 $(F - E_1) = (R_1 - E_2) = (R_2 - S) = P$

Note: each difference is equal to P (look on the flow sheet where those *differences* are).

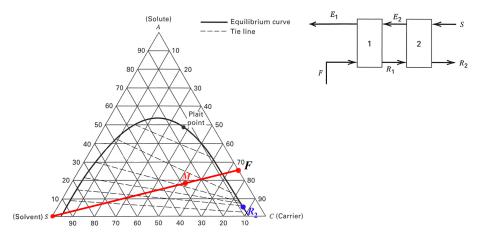


Rearranging again:

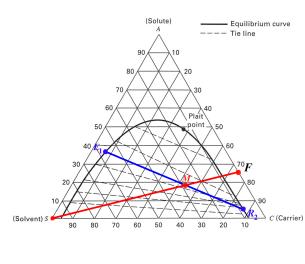
$$F + P = E_1$$
$$R_1 + P = E_2$$
$$R_2 + P = S$$

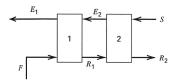
Interpretation: P is a fictitious operating point on the ternary diagram (from lever rule)

- P connects F and E₁
- ▶ P connects R₁ and E₂
- P connects R_2 and S



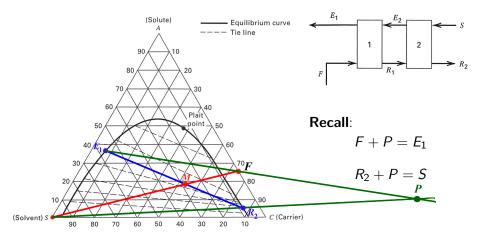
For example, let's require $x_{R_2,A} = 0.05$ (solute concentration in raffinate). What is $y_{E_1,A}$ then (concentration of solute in the extract)?





Note: the line connecting E_1 to R_2 is not a tie line. We use the lever rule and an overall mass balance $(F + S = E_1 + R_2)$ to solve for all flows and compositions of F, S, E_1 , and R_2 .

 $y_{E_1,A} \approx 0.38$ is found from an overall mass balance, through *M*.



Extrapolate through these lines until intersection at point P. Minimal achievable E_1 concentration? mentally move point M towards S. What happens to P? Alternative (simpler?) explanation on next slide.

42