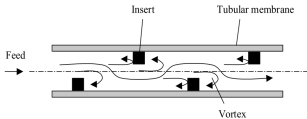


# Fouling

- ▶ Process feed pretreatment is important.
- ▶ e.g. in bio area: prefiltration, pasteurisation to destroy bacteria, or adjust pH to prevent protein precipitation
- ▶ Backflushing mostly restores permeation rate (opens pores)
- ▶ Can also use pulsated/oscillating feed flows
- ▶ Consider adding tube inserts



- ▶ Inject air: *sparging* with oxygen or nitrogen
- ▶ Oscillating electrical field works on certain feeds
- ▶ Chemical cleaning is eventually required [long time], e.g.:
  - ▶ flush with filtered water
  - ▶ recirculate/back-flush with a cleaning agent at high temperature
  - ▶ rinse to remove the cleaning agent
  - ▶ sterilize by recirculating weak chlorine solution at high temps
  - ▶ flushing with water to remove sterilizing solution

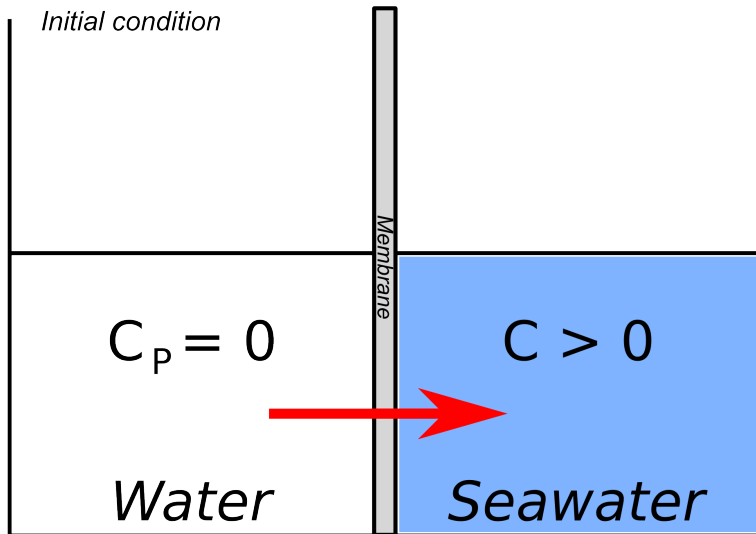
## Video

[http://www.youtube.com/watch?v=YIMGZWmh\\_Mw](http://www.youtube.com/watch?v=YIMGZWmh_Mw): How spiral membranes are made

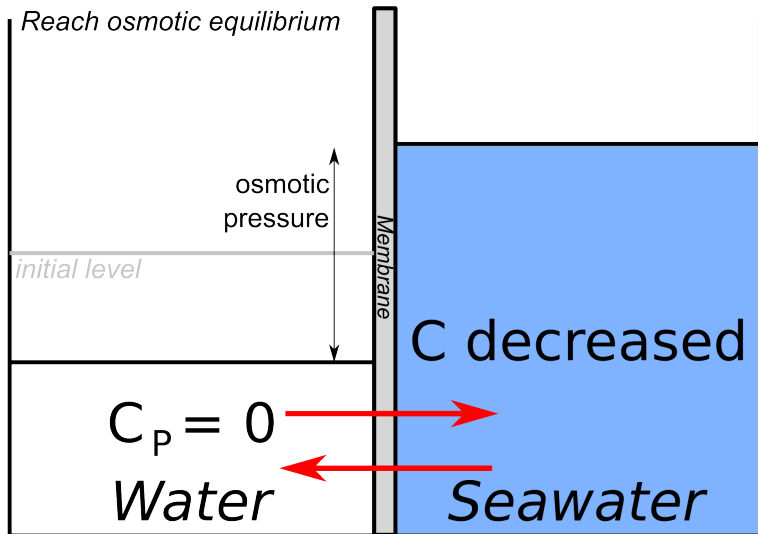
# Reverse osmosis

- ▶ One the most requested topics (start of the term!)
- ▶ One of the largest membrane markets by \$ size
  1. Dialysis
  2. Reverse osmosis (water treatment)
- ▶ What is osmosis? [Greek = “push”]
- ▶ Then we look at reverse osmosis (RO)
- ▶ Applications of RO
- ▶ Modelling RO

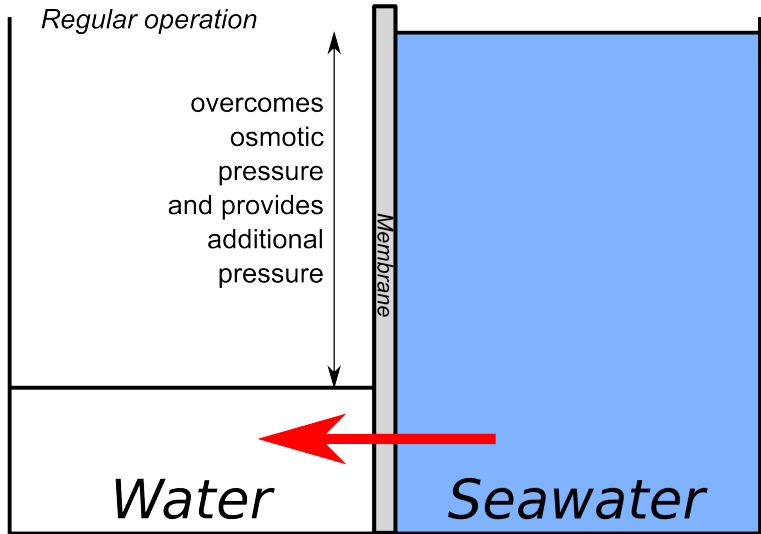
## Osmosis principle



## Osmosis principle



## Reverse osmosis principle

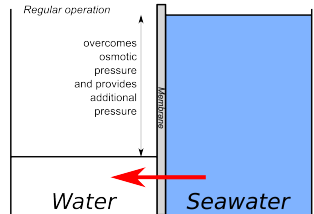


## (Reverse) Osmosis principle

- ▶ Assume solute barely passes through membrane ( $C_p \approx 0$ )
- ▶ but solvent passes freely: this is why we call it a *semipermeable membrane*
- ▶ Chemical potential drives pure solvent (water) to dilute the solute/solvent (mixture).
- ▶ This *solvent flux* continues until equilibrium is reached
  - ▶ solvent flow to the left equals solvent flow to the right
  - ▶ results in a pressure difference (head)
  - ▶ called the *osmotic pressure*  $= \pi$  [Pa]
  - ▶ a thermodynamic property  $\neq f(\text{membrane})$
  - ▶ a thermodynamic property  $= f(\text{fluid and solute properties})$ , e.g. *temperature, concentration, pressure*

# (Reverse) Osmosis principle

- ▶ Osmosis in action:
  - ▶ trees and plants to bring water to the cells in upper branches
  - ▶ killing snails by placing salt on them
  - ▶ why freshwater fish die in salt water and *vice versa*
  - ▶ try at home: place peeled potato in very salty water
- ▶ If you exceed osmotic pressure you reverse the solvent flow
- ▶ Called “reverse osmosis”
- ▶ Net driving force in this illustration = \_\_\_\_\_





# Typical values of osmotic press

For dilute solutions

$$\pi \approx \frac{nRT}{V_m} = CRT$$

$\pi$	[atm]	osmotic pressure
$n$	[mol]	mols of <b>ions</b> : e.g. $\text{Na}^+$ and $\text{Cl}^-$
$R$	$[\text{m}^3 \cdot \text{atm} \cdot \text{K}^{-1} \cdot \text{mol}^{-1}]$	gas law constant: $8.2057 \times 10^{-5}$
$V_m$	$[\text{m}^3]$	volume of solvent associated with solute
$T$	[K]	temperature
$C$	[mol of ions per $\text{m}^3$ ]	generic concentration

## Example

Prove to yourself: 0.1 mol ( $\sim$  1 teaspoon) of NaCl dissolved in 1 L of water at 25°C is **4.9 atm**!

- ▶ that's almost 500 kPa
- ▶ or almost 50m of head for 5.8 g NaCl in a litre of water
- ▶ (recall: 1 atm  $\approx$  10 m of water height)

## Other osmotic values

The previous equation is an approximation.

Some actual values:

Substance	Osmotic pressure [atm]
Pure water	0.0
0.1 mol NaCl in 1 L water	4.56
2.0 mol NaCl in 1 L water	96.2
Seawater [3.5 wt% salts]	25.2

- ▶ Driving force in membrane separation is pressure difference
- ▶  $\Delta P = \pi$  implies we only counteract the osmotic pressure
- ▶ Reverse osmosis occurs when we increase  $\Delta P > \pi$
- ▶ So the net useful driving force applied:  $\Delta P - \pi$
- ▶ Ultrafiltration  $\Delta P$  was 0.1 to 1.0 MPa (10 atm) typically
- ▶ RO: typical  $\Delta P$  values: 2.0 MPa to 8.0 MPa, even 10.5 MPa

## Let's be a little more accurate

- ▶ The solute (salt) passes through the membrane to the permeate side
- ▶  $C_p \neq 0$
- ▶ There is an osmotic pressure,  $\pi_{\text{perm}}$  back into the membrane.
- ▶ Correct, net driving force =  $\Delta P - \Delta\pi$ 
  - ▶  $\Delta P$  is the usual TMP we measure
  - ▶  $\Delta\pi = \pi_{\text{feed}} - \pi_{\text{perm}}$
  - ▶  $\Delta\pi = C_{\text{ions,feed}}RT_{\text{feed}} - C_{\text{ions,perm}}RT_{\text{perm}}$
  - ▶ Even more correctly:  $\Delta\pi = C_{\text{ions,wall}}RT_{\text{wall}} - C_{\text{ions,perm}}RT_{\text{perm}}$

### Key point

There's a natural limitation here: what if we try to recover too much solvent?

# Widest application for RO: desalination

Some quotes:

- ▶ *"McIlvaine forecasts that world RO equipment and membrane sales will reach \$5.6 billion (USD) in 2012, compared to \$3.8 billion in 2008 (actual)."*
- ▶ *"Depleting water supplies, coupled with increasing water demand, are driving the global market for desalination technology, which is expected to reach \$52.4 billion by 2020, up 320.3% from **\$12.5 billion in 2010**. According to a recent report from energy research publisher SBI Energy, membrane technology reverse osmosis will see the largest growth, reaching \$39.46 billion by 2020."*

# Industrial applications of RO

- ▶ demineralization of industrial water before ion exchange
- ▶ not primary aim, but RO membranes retain  $> 300$  Dalton organics
- ▶ ultrahigh-purity water
  - ▶ laboratories
  - ▶ kidney dialysis
  - ▶ microelectronic manufacturing
  - ▶ pharmaceutical manufacturing (purified water)
- ▶ tomato, citrus, and apple juice dewatering [ $\sim 4.5$  c/L; 1995]
- ▶ dealcoholization of wine and beer to retain flavour in the retentate
- ▶ other: keep antifreeze, paint, dyes, PAH, pesticides in retentate; discharge permeate to municipal wastewater

# Salt-water reverse osmosis example



- ▶ Larnaca, Cyprus [island state near Greece/Turkey]
- ▶ Desalination plant: Build, Own, Operate, and Transfer
- ▶ 21.5 million m<sup>3</sup> per year
- ▶ Seawater intake → flocculation and filtration [why?] → RO  
→ chemical dosing → chlorination
- ▶ Energy recovery of  $\Delta P$  (see <http://www.youtube.com/watch?v=M3mpJysa6zQ>: novel

way of recovering pressure energy)

## RO costs [Perry's; 8ed], 1992

Household RO  
cost:

- ▶ \$ 0.015 to \$0.07/L

**TABLE 20-23 Representative RO Process Costs**

Costs	Seawater
Operating conditions	
Inlet pressure	6.9 MPa
Flux	25 LMH*
Conversion	40%
Total cost, \$/1000 gal	4.7
Capital cost	2.1
Operating cost	2.6
Total capital cost, \$/(gal/day)	4.5
Direct costs	3.7
Equipment	3.3
Indirect costs	0.8
Total operating cost, \$/1000 gal	2.6
Energy	1.6
Membrane replacement	0.4
Chemicals	0.2
Labor	0.3
Other	0.1